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The Specific Heat at Constant Volume of para-Hydrogen at Temperatures from 15 to 90° K and Pressures to 340 atm

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THE computation of thermodynamic properties, relative to that of ideal gas, of compressed fluid by means of the equation of state data requires the data to be extremely accurate. The uncertainties that are introduced through the derivatives of the equation of state would be minimized by supplementing the calculations with the constant volume specific heat data of the compressed fluid. Specific heats for both ideal gas and compressed liquid states, together with PVT data, will permit computations around closed paths to check the overall consistency of the data. For these applications our current programme on hydrogen properties includes calorimetric specific heats of parahydrogen at constant volume. There are reported in this paper measurements of $C_{\rm v}$ of the compressed fluid from well below to above the critical temperature.

Experimental procedure

The descriptions of apparatus and sample preparation have been published.^{1,3} The calorimeter consists of a spherical stainless steel sample container of 72 cm³ volume with a platinum resistance thermometer, heater windings, and difference thermocouples attached. The container was suspended by a filling capillary inside an adiabatic shell which in turn was mounted in a cryostat.

The hydrogen sample is 20° K equilibrium hydrogen prepared from electrolytic hydrogen as previously described. The chemical impurities present in the hydrogen sample are estimated to be less than 0.01 per cent based on tests made by the supplier (National Cylinder Gas Co.). The isotopic content is estimated from a knowledge of the process of preparation of the hydrogen gas to be the same as that of naturally occurring hydrogen. The para-hydrogen concentration at the beginning of a run is estimated to be in excess of 99 per cent, based on the iron oxide catalyst temperature and the indication from a thermal conductivity analyser. In preliminary studies the conversion rate of para- to ortho-hydrogen at pressures up to 300 atm was of the order of I per cent per day at 76° K.

The desired filling density was determined approximately from the PVT data of this laboratory.² The actual

amount of sample was measured at the end of each run by gasometry³ and this value was used in calculations of the density and the specific heats. An adjustment was made for the gas contained in the filling capillary. This adjustment, however, was extremely small and could have been neglected. Adjustment was also made for the change in volume with temperature and pressure. The maximum adjustment in density from all these sources during a run was less than 0.5 per cent. The true density associated with each specific heat value was thus calculated from the actual amount of sample in the sample container, V = V(T, P).

Heat capacity measurements were made as a function of temperature at nearly constant density. An adjustment was made to the measured value of specific heat \bar{C}_{v} , for the work done by the fluid as it expanded. This adjustment, developed by Walker,⁴ is

$$\Delta C_{\rm v} = -\frac{1}{N} \left[T \left(\frac{\Delta P}{\Delta T} \right)_{\rm v} + \frac{\Delta P}{2} \right] \frac{\Delta V}{\Delta T} \qquad \dots (1)$$

 $\Delta C_{\rm v}$ is added to $\bar{C}_{\rm v}$ to obtain the adjusted value $C_{\rm v}$. The calculated increase in pressure during the heating interval is ΔP , ΔV is the corresponding increase in volume, $(\Delta P/\Delta T)_{\rm v}$ was calculated from PVT data, and N is the amount of sample in the container. This adjustment was always less than 1 per cent of the measured value.

The heat capacity of the sample was taken to be the difference between the total heat capacity and the heat capacity of the sample container. The adjustment for curvature was found to be negligible in these measurements. The heat capacity of the sample container was measured at 35 temperatures between 15 and 100° K and fitted with two polynomials by least squares. Below 26° K a polynomial of 6 terms was used and above 26° K a polynomial of 7 terms. The first and second derivatives of the two polynomials at 26° K agreed to within 0.03 per cent and the r.m.s. per cent deviation of the measured values from the polynomial representations was 0.12 per cent.

A platinum resistance thermometer, calibrated on the NBS-1955 temperature scale by the NBS Heat Division in Washington, D.C., was used to measure T and ΔT .

Table 1. Experimental Data. Specific Heat, Temperature, Density, and Pressure

	P (atm)	Density (mole/cm³)	C _v (J/mole deg.)	<i>T</i> (°K)		P (atm)	Density (mole/cm³)	C _v (J/mole deg.)	<i>T</i> (° K)
	22.70	0.02700	10.27	16.120		49.76	0.03788	11.31	 19·916
ĺ	23.70	0.03790	10.37	16.139		67·81			
	36.03	0.03790	10.92	18.404			0.03787	11.71	21.863
	55.15	0.03789	11.46	20.481		72·61	0.03787	11.80	22.377
	69.63	0.03788	11.74	22.038		87.03	0.03786	12.06	23.924
-	88.75	0.03787	12.09	24 088		105.77	0.03785	12.39	25.930
	107.90	0.03786	12:41	26.136		125.48	0.03784	12.67	28.037
	126.84	0.03785	12.68	28.160	Run 1	144-41	0.03783	12.92	0.060
1	145.89	0.03784	12.92	30.196		163-29	0.03782	13.15	2.082
Run	164.98	0.03783	13.16	32.239		181.71	0.03781	13.35	4.056
	183.79	0.03782	13.37	34.255		197-41	0.03781	13.51	5.742
	199.85	0.03781	13.52	35.982		214.03	0.03780	13.65	7.538
	218.08	0.03780	13.69	37.951		272.42	0.03777	14.08	3.923
ļ	236.43	0.03780	13.82	39.930					
	254.58	0.03779	13.95	41.911					
1	272.69	0.03778	14.08	43.900		14.56	0.01619	18.64	3.889
	290.82	0.03777	14.22	45.902		18.88	0.01619	15.21	6.035
	309.13	0.03777	14.35	47.938		23.28	0.01618	14.38	8.194
						31.64	0.01618	13.81	2.244
	327-42	0.03776	14·49	49.992		35.79	0.01618	13.69	4.245
	19.05	0.02545	13.19	33.107	Run 2	39.78	0.01618	13.63	6.166
	23.96	0.02545	13.18	34.245	Ruii 2	47·73	0.01618	13.61	9.986
	25.62	0.02545	13.20	34.622		68.32		14.83	
1	29.13	0.02545					0.01617	12.03	9.894
,		0.02545	13.19	35.434		89.06	0.01616	13.92	9.931
	35.64	0.02545	13.21	36.926		109.80	0.01615	16.10	0.052
_	37.51	0-02545	13.23	37.354		129.91	0.01614	17.70	9-943
Run	46.04	0.02544	13.28	39.301					
	53.96	0.02544	13.33	41.109		27.42	0.03/5/	1.24	0.110
	74.75	0.02543	13.45	45.860		27.62	0.03676	11.34	0.140
	83.86	0.02543	13.55	47.949		45.91	0.03675	11.80	22.205
	93.05	0.02542	13.63	50-060		62·16	0.03674	12:11	24.028
	135.28	0.02541	14.25	59.845	i I	63.53	0.03674	12-13	24.182
	179.75	0.02539	15.34	70.316		80.54	0.03674	12.41	26.087
	217.94	0.02537	16.65	79.472		98.79	0.03673	12.67	28-132
1	259.83	0.02535	18.31	89.674		116.74	0.03672	12.90	30-145
						134.52	0.03671	13.15	32-142
	11.03	0.03072	12.55	27.532		152-14	0.03670	13.30	34-124
	24-44	0.03072	12.70	29.628	Run 3	169-18	0.03669	13.48	6.050
	40.97	0.03071	12.95	32.215		186-11	0.03668	13.63	7.971
	54.04	0.03070	13.12	34.262		203-41	0.03668	13.76	9.944
}	67.30	0.03070	13.26	36-344		220.59	0.03667	13.87	1.916
	80.57	0.03069	13.37	38.439	ļ	237.85	0.03666	14.00	3.909
	93.60	0.03069	13.47	40.505		255.17	0.03665	14-12	5.923
Rur	106.09	0.03068	13.54	42.494		272.73	0.03664	14.26	7.978
Kui	114.75	0.03068	13.64	43.881		290.16	0.03664	14.39	0.029
		0.03067		45.898		306.98	0.03662	1 4	
į	127.31	0.03067	13.74	47.880		324.33		14.52	2.051
	139.58		13.86			324.33	0.03662	14.67	4.085
	151-89	0.03066	13.97	49.879					
İ	213.71	0.03063	14.69	60.070		70.00	0.02026	10.72	0.031
	268.76	0.03061	15.63	69.365		70.88	0.03936	10.73	8.021
	327.68	0.03058	17.04	79·554		90.41	0.03935	11.23	20.048
		004	. m			109-45	0.03934	11.66	21.999
	13.25	0.01095	17.56	33.497		129.00	0.03933	12.02	3.985
1	14.77	0.01095	16.07	34.695		148-56	0.03932	12.36	25.963
	16.87	0.01095	15.09	36.367		168.05	0.03931	12.64	7.931
1	19.09	0.01095	14.52	38-150		187-65	0.03930	12.90	9.909
İ	21.51	0.01095	14-14	40-105	Run 4	207-42	0.03929	13-14	1.907
1	24.25	0.01095	13.88	42.325		227.23	0.03928	13.36	3.907
Rur	26.98	0.01095	13.69	44.538		246.87	0.03927	13.57	35·894
1	29.54	0.01094	13.61	46.624	:	267.28	0.03926	13.74	7-971
	31.97	0.01094	13.56	48.607		286-47	0.03925	13.88	9.935
Í	34.36	0.01094	13-57	50· 5 55		305.56	0.03924	14.02	11.897
	45.59	0.01094	13.77	59.757	i	324.96	0.03924	14.16	13.899
i	58.30	0.01094	14.68	70.241		344.48	0.03924	14.31	45·915
1	20 30	0 01074	14 00	10241	I	277 7 0	0 03723	1131	0 110



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Table 1-continued

	P (atm)	Density (mole/cm ³)	$C_{\rm v}$ (J/mole deg.)	T (°K)
	13.60	0.01869	17:36	33.316
	16.28	0.01869	15.47	34-425
	20.71	0.01869	14.46	36.217
	25.60	0.01868	14.01	38-159
	30.39	0.01868	13.78	40.040
	35.33	0.01868	13.66	41.969
Run 9	40.59	0.01868	13.57	44.018
	46.06	0.01868	13.55	46.142
	51.47	0.01868	13.54	48.238
	56-66	0.01867	13.57	50.249
	82.68	0.01866	14.01	60.335
	105-92	0.01866	14.81	69-404
	132.60	0.01864	16-18	79.924
	156-24	0.01863	17.59	89-331
	16.97	0.02291	13.81	33-696
	24.84	0.02291	13.51	35-943
	39.39	0.02291	13.38	40.010
	46.36	0.02290	13.38	41-943
	53.43	0.02290	13.39	43.900
Run 10	60.94	0.02290	13.45	45-976
	68-41	0.02290	13.49	48.043
	75.79	0.02289	13.59	50.086
	111-49	0.02288	14.15	60.017
	146-33	0.02287	15·10	69.823
	181.51	0.02285	16.55	79.870
	217-63	0.02283	18.26	90.319

	P (atm)	Density (mole/cm³)	$C_{\rm v}$ (J/mole deg.)	<i>T</i> (° K)
	198·83 219·32 241·49	0·04181 0·04180 0·04179	11·52 11·91 12·29	21·991 23·917 25·987
Run 11	263.73	0.04177	12.62	28.055
	285-30	0.04176	12.91	30.055
	306.77	0.04175	13.18	32.046
	327.74	0.04174	13.41	33-990
	14.72	0.01329	17-67	34-216
	18-19	0.01329	15.27	36.402
	21.32	0.01329	14.56	38.384
	24-22	0.01329	14.15	40.214
	27.21	0.01329	13.92	42.107
	30.18	0.01329	13.77	43.985
Run 12	33.27	0.01329	13.68	45.940
	36-52	0.01329	13.61	47-994
	39.78	0.01328	13.60	50.057
	55.24	0.01328	13.88	59.868
	71-10	0.01327	14.68	69.974
	87:01	0.01327	16.03	80.206
	102-24	0.01326	17.57	90.055

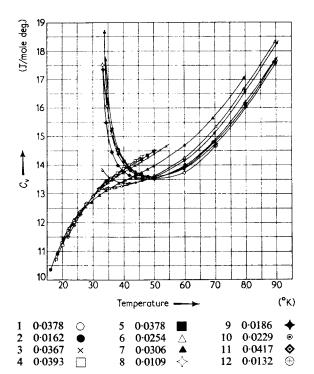


Figure 1. Specific heat as a function of temperature for several densities. The run numbers are given above and the densities are in mole/cm³

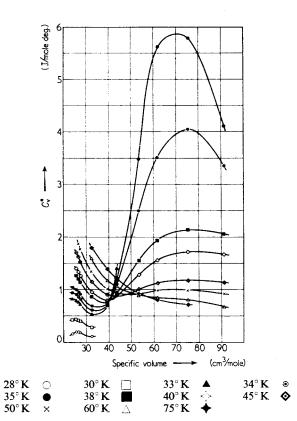


Figure 2. Residual specific heat as a function of specific volume for several temperatures

Experimental results

Table 1 lists the adjusted values of the specific heat of para-hydrogen. The temperature is the average of the sample container temperatures which were measured before and after the heating interval and extrapolated to the middle of the heating time interval. Figure 1 shows the specific heat as a function of temperature for each run.

Figure 2 shows the residual specific heat versus specific volume for several isotherms. The residual specific heat is defined as

$$C_{v}^{*}(v,T) = C_{v}(v,T) - C_{v}^{\circ}(T)$$
 ...(2)

where $C_v^\circ(T)$ is the 'ideal gas' value. This residual arises from molecular interaction. The high maximum in the 34° K isotherm occurs approximately at the critical volume, as expected. The spacing of the data in density precludes locating this maximum accurately. An interesting feature of this surface is another maximum at low specific volume. The suggested shape of a general $C_v^*(v,T)$ surface due to Rowlinson, based on measurements of several authors, does not have this last feature. At large values of the volume, C_v^* approaches zero as v increases, since the real gas properties approach the ideal at low density.

Analysis of results

The values of C_v have an estimated uncertainty of 0.3 per cent below 50° K with the exception of the lower density runs 2, 8, 9, and 12 where the uncertainty may be as large as several per cent near the critical temperature. The uncertainty in C_v in the region above 50° K may be as large as 0.5 per cent.

The ratio of the sample heat capacity to the gross heat capacity varies from 0.94 at the low temperature, high density case to 0.28 at the high temperature, low density case.

The reproducibility of the data is indicated by runs 1 and 5 for which the filling conditions were duplicated. The agreement, in this somewhat favourable case, in C_v from the two runs is within 0.2 per cent.

A test of the capability of the calorimeter was made by measuring the specific heat of solid argon and comparing the results to the extensive data of Flubacher, Leadbetter, and Morrison. Both sets of data were smoothed and the percentage difference was computed at every 5° K from 20 to 60° K. The r.m.s. percentage difference was 0.35 per cent. The measurements of this laboratory on solid argon were reported in reference 1.

The residual specific heat may be also calculated from PVT data according to the relation⁶

$$C_{\mathbf{v}}^{*}(v,T) = T \int_{\infty}^{v} \left(\frac{\partial^{2} P}{\partial T^{2}}\right)_{\mathbf{v}} dv \qquad \dots (3)$$

The PVT data on para-hydrogen of this laboratory are not yet in final form to carry out this calculation to compare

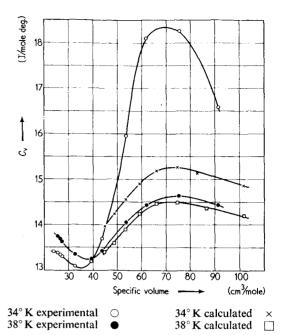


Figure 3. Comparison of specific heats calculated from PVT data and specific heats measured directly by calorimetry

with that obtained calorimetrically. Obviously great care must be taken with the representation of the PVT data if the second derivative in equation (3) is to be reliable. Preliminary comparison was made at a few points using the PVT data for normal hydrogen.⁵ An equation equivalent to equation (3) using the smoothed values of $(\partial Z/\partial T)_v$ and $(\partial^2 Z/\partial T^2)_v$, where Z = PV/RT, was used. The 'ideal gas' values for para-hydrogen were used for $C_v^\circ(T)$. The results for the 34 and 38° K isotherms are shown with the measured values of C_v in Figure 3. The agreement is quite reasonable, with most of the disagreement due to uncertainties in the derivatives of Z. For the 34° K isotherm,

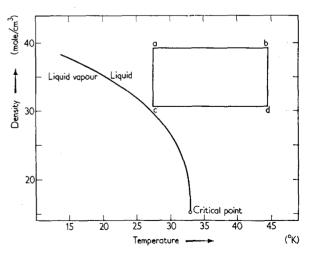


Figure 4. Path of integration for entropy calculations

which is only slightly above the critical temperature, some of the disagreement may be due to non-equilibrium experimental conditions. Equilibrium in the region of the critical point is known to be sluggish. Large deviations near the critical density as seen in Figure 3 have also been observed in carbon dioxide in the work of Michels and Strijland.⁷

A check on the internal consistency of the C_v and PVT measurements was made by calculating the entropy changes in a closed loop consisting of two isochores and two isotherms as shown in Figure 4. The entropy change along an isotherm was calculated by numerically integrating $(\Delta P/\Delta T)_v$ with respect to specific volume. The quantity $(\Delta P/\Delta T)_v$ is approximated from a preliminary smoothing of the PVT data of this laboratory. The change in entropy along an isochore was calculated by integrating smoothed values of C_v/T . The results, which indicate good internal consistency, are summarized in Table 2.

The densities and pressures listed with the values of specific heat are accurate to within 1 part in 500.

This report represents part of a programme on thermodynamic properties of *para*-hydrogen under the direction of R. D. Goodwin. Acknowledgement is made to R. D. Goodwin, L. A. Weber, and H. M. Roder who have made numerous experimental and computational contributions. This work was supported by the U.S. National Aeronautics and Space Administration.

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Table 2

Path	ΔS (J/mole deg.)
a to b	6.012
b to d	5.602
d to c	-5.870
c to a	-5.757
Total	-0.013